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A STATISTICAL DEFINITION OF PERFECT MIXTURES OF SOLIDS OF DIFFERENT SIZES

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When mixing solids, it is desirable to be able to evaluate the performance of a mixer in terms of its ability to produce mixtures that approach the theoretical limit of uniformity. Although a satisfactory correlation exists for mixtures where the particles are of uniform size, none has yet been developed for multisized particles. A mathematical definition of a perfect mixture of three sizes of particles is proposed. The principles employed can be extended to any number of sizes, but the complexity of the equations increases rapidly. Agreement with experimental results appears substantially better than that obtained by previous investigators.

TWO MODELS have been used in attempting to define perfect mixtures of solids. Manning (9), Lacey (8), Buslik (4), Stange (13), and others (10, 14) have used the statistical approach, defining mixing in terms of the standard deviation of the composition of samples. Hemelrijk (7) and Blumberg and Maritz (2) used the chi-square distribution for the statistical analysis, but otherwise followed essentially the same approach. On the other hand, Brothman, Wollan, and Feldman (3) and Coulson and Maitra (5) used a kinetic approach based on shear mixing process, which they described as three-dimensional shuffling. Oyama (11) attempted a third approach, and defined as a criterion the specific volume of the mixture of two different sizes of particles. This criterion, however, is demonstrably unreliable since packing arrangement rather than particle distribution is important.

The most common definition of a complete mixture is that which might be obtained by distributing its component particles with equal probability of occupying any position throughout the system. This form of mixing may sometimes produce very poor results in that the mixture is far from homogeneous. Hence, it may be more satisfactory to apply the term complete to the mixing process itself rather than to the resulting mixture. This makes an allowance for the fact that a complete mixing process can still produce bad mixtures. For this reason it has been proposed to replace complete mixing by the term random, which describes the situation more realistically, and we use the term random mixing process instead of mixing. Buslik, Blumberg and Maritz, and Hemelrijk based their statistical consideration on the following definition (7): "A mixing process is called random if all particles are distributed independently in the mixture in such a way that, for every component of the mixture, the probability of finding a particle of this component at a given point is the same for all points in the mixture." The above statement will serve to define our use of the term random, either when used in referring to a random mixture or when speaking of a random distribution.

If a mixture is composed of particles of a single size, Lacey (8) and others (4, 9) showed that if the mixture is random, the standard deviation of the composition of samples is equal to the standard deviation that is obtained by applying the binomial distribution:

$$\sigma = \sqrt{\frac{P(1-P)}{n}} = \lim_{N \rightarrow \infty} \sqrt{\frac{\sum_i (x_i - x)^2}{N}} \quad (1)$$

where n = the number of particles in a sample, x = over-all particle fraction of one component in a mixture, x_i = particle fraction of one component in the i th sample, P = the ratio of

the number of particles of a component to the total number of particles in the mixture, and N is defined as the number of samples analyzed.

Mixtures of nonuniform sizes of particles, however, proved less tractable to theoretical definition. Manning (9) attempted to use his equation for multisized particles, but the relation does not agree well with experimental results. Manning used Equation 1 in the form of

$$\sigma = \sqrt{\frac{S(1-S)w}{W}} \quad (2)$$

where S is the weight fraction of large particles, w is the weight of a particle, and W is the weight of each sample. Manning used this equation for the large particles. For mixtures of large and medium particles, he used the following:

$$\sigma_y^2 = \sigma_x^2 - \sigma_{x+y}^2 \quad (3)$$

where σ_x^2 and σ_y^2 are the variances of large and medium particles, respectively, and σ_{x+y}^2 is the variance of mixtures of large and medium particles.

Buslik modified Manning's model as follows: He assumed every component to be distributed binomially, and he divided the whole mixture into equal subvolumes which he called units. According to the derivation of his equation, each size is binomially distributed throughout the volume of the mixture, with a variance given by:

$$\sigma_a^2 = \frac{A(1-A)w_a + A^2(w - w_a)}{W} \quad (4)$$

where w_a is the average particle weight in the size fraction being considered (constant density is assumed), \bar{w} is the average particle weight in the whole mixture, calculated from $\bar{w} = Aw_a + Bw_b + Cw_c$, etc., and A, B, C , etc., are the fractions by weight of particle sizes w_a, w_b, w_c , etc. W is the total sample weight, and A is the weight fraction being considered.

Although Buslik's model, as expressed in Equation 4 was a substantial improvement on Manning's and gave good results for the large size particle, it was in poor agreement for the smaller sizes.

The failure of Buslik's model appears to stem from an important omission—that is, he does not consider the existence of gaps between large particles in which only small particles can fit. If several sizes of particles are mixed, and if the largest size is randomly distributed, it follows that some of the large particles will be so close together that medium-sized particles cannot fit between them. This volume is not avail-

able to the medium particles, and the volume in which the latter can be randomly mixed is correspondingly smaller. This error is corrected in the model proposed below. Although the proposed method may be extended to any number of particle sizes, its complexity increases rapidly. Hence, it is presented here for only three sizes of particles.

If we consider a mixture that has X , Y , and Z volume fractions of large, medium, and small particles, respectively, the model proposes that, because of their greater mass, the large particles will be unaffected by the smaller particle sizes, except that the latter will provide support. Then, as with Buslik's model, the variance of the large particle content in equal-sized samples is

$$\sigma_x^2 = \sum_{i=1}^{\infty} P_i(x - x_i)^2 \cong \frac{x(1-x)}{a} \quad (5)$$

where

x = volume fraction of large particles in the mixture

x_i = volume fraction of large particles in the i th sample

P_i = probability of having a volume fraction X_i in the sample

a = the ratio of the sample volume to the volume of one large particle

Unless one can cut through particles in the sampling process, the number of particles in a sample is an integer, and hence the x_i 's are binomially distributed. Thus, unless the sample volume is large compared with the particle size, the inequality in Equation 5 may be important. The magnitude of this inequality is the subject of another study now in progress.

It is now necessary to determine the amount and probability distribution of the space between large particles in which medium particles will not fit. This space, which we designate as excluded volume, is determined below for a simplified model.

Consider a mixture of spherical particles in a spherical sample volume. When two large particles are so close that a medium one cannot fit between them, we may approximate the excluded volume as a cylinder of length and radius $(h - r_m)$ as shown in Figure 1. If we choose to keep one of the large particles fixed in space and allow the other to occupy all positions which will produce a nonzero excluded volume, then the excluded volume is given by the equation

$$V_{\text{ex}1} = \Pi(h - r_m)^2 l, \quad 0 < l < 2r_m \quad (6)$$

where

$$h = \sqrt{(r_l + r_m)^2 - \left(r_l + \frac{l}{2}\right)^2} = \frac{1}{2} \sqrt{\alpha - \beta l - l^2} \quad (7)$$

in which we define α , β , and γ as follows:

$$\alpha = 8r_m r_l + 4r_m^2$$

$$\beta = 4r_l$$

$$\gamma = 2r_m$$

In the above set of equations, l is a variable that has meaning for any value between zero and $2r_m$. The probability that l be of a given length is not the same for all lengths. To determine the probability distribution $f(l)$, one must go back to the original premise that one large particle is kept fixed, and that the other is allowed to occupy, with equal probability, all positions which will produce a nonzero volume. Then, since the probability that the centers of the two large particles be a distance R apart is proportional to R^2 , one may see that the distribution function $f(l)$ is expressed by

$$\int_0^{2r_m} f(l) dl = \int_0^{2r_m} \frac{4\pi(2r_l + l)^2 dl}{\bar{V}_v} = 1, \quad 0 \leq l \leq 2r_m \quad (8)$$

where the range of definition has been limited to values of l in which excluded volumes occur, and

$$\bar{V}_v = \frac{4}{3} \pi (2r_l + 2r_m)^3 \quad (9)$$

hence,

$$f(l) = \frac{4\pi}{\bar{V}_v} (2r_l + l)^2, \quad 0 \leq l \leq 2r_m \quad (10)$$

The expected volume excluded to medium particles between two large particles is thus

$$E(V_{\text{ex}1}) = \int_0^{2r_m} V_{\text{ex}1} f(l) dl \quad (11)$$

Substituting Equations 6, 7, and 10 into Equation 11, one gets

$$E(V_{\text{ex}1}) = \frac{\pi^2}{\bar{V}_v} \int_0^{2r_m} \left[(\alpha + \gamma^2)l - \beta l^2 - l^3 - 2\gamma l \times \sqrt{\alpha - \beta l - l^2} \right] \left(\frac{\beta^2}{4} + \beta l + l^2 \right) dl \quad (12)$$

By integrating and rearranging, we get

$$E(V_{\text{ex}1}) = \frac{\pi^2}{\bar{V}_v} \left[(21.33r_m^6 + 74.97r_m^5 r_l + 69.33r_m^4 r_l^2 + 21.33r_m^3 r_l^3) - 2\sqrt{\alpha} (4.27r_m^5 + 17.07r_m^4 r_l + 23.47r_m^3 r_l^2 + 13.3r_m^2 r_l^3 - 24r_m r_l^4) + 16r_m r_l (r_m + r_l)^2 \left(\frac{\pi}{2} - \sin^{-1} \frac{r_l}{r_m + r_l} \right) \right] \quad (13)$$

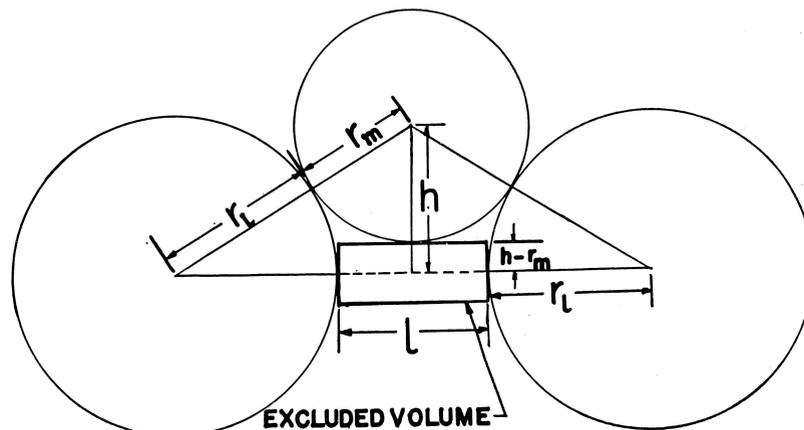


Figure 1. Geometrical model for excluded volume between two large particles

When we consider more than two particles, there are several possible arrangements that yield excluded volumes. We may consider the geometrical arrangements giving excluded volumes between three particles to fall into two distinct types: 1. Three particles are placed so that the space between each of the three pairs contains an excluded volume. 2. Two particles are close enough to produce an excluded volume, while the third is so placed as to have an excluded volume with either of the other two or with neither, but not with both.

Arrangements of Type 2 are considered two-particle interactions. When considering the excluded volume produced by Type 1 interactions, it is necessary to account only for those excluded volumes which have not been previously accounted for as two-particle interactions. For example, if three large particles, A, B, and C, interact to form excluded volumes between A and B, between A and C, and between B and C, the interactions of A with B and of B with C are accounted for as Type 2 interactions.

The Type 1 interaction in a three-particle group out of a total of m large particles is the interaction between particles A and C. Let $E(V_{\text{ex}})_{A/B \leftrightarrow C}$ denote the expected excluded volume resulting from this interaction. The ratio of $E(V_{\text{ex}})_{A/B \leftrightarrow C}$ to the expected excluded volume between particles A and B—i.e., $E(V_{\text{ex}})_1$ may be expressed as the ratio of probabilities of the conditions that the excluded volumes might occur. That is

$$\frac{E(V_{\text{ex}})_{A/B \leftrightarrow C}}{E(V_{\text{ex}})_1} = \frac{\Pr[l_2 < d_m/l_1 < d_m]}{\Pr[l_1 < d_m]} \quad (14)$$

where l_1 = the distance between particles A and B
 l_2 = the distance between particles A and C

On the other hand, the probability that particle C is so located as to produce an excluded volume between A and C is a function of the volume around A which is not occupied by other particles. Let a_2 be the ratio of the probability that l_2 is less than d_m when l_1 is also less than d_m divided by the probability that l_1 is less than d_m , then

$$a_2 = \frac{\Pr[l_2 < d_m/l_1 < d_m]}{\Pr[l_1 < d_m]} = \frac{\left[4\pi(d_l + d_m)^2 - \frac{\pi}{4}d_l^2\right](m-2)}{[4\pi(d_l + d_m)^2(m-1)]} \quad (15)$$

Combining 14 and 15 one can write

$$E(V_{\text{ex}})_{A/B \leftrightarrow C} = a_2 E(V_{\text{ex}})_1 \quad (16)$$

Therefore, the total expected excluded volume caused by particle A in a three-particle group is expressed as $E(V_{\text{ex}})_2$ and has the value

$$E(V_{\text{ex}})_2 = E(V_{\text{ex}})_1(1 + a_2) \quad (17)$$

Similarly, if four particles, A, B, C, and D, are involved, the contribution of one particle is:

$$\begin{aligned} E(V_{\text{ex}})_3 &= E(V_{\text{ex}})_2 + a_3 E(V_{\text{ex}})_1 \\ &= E(V_{\text{ex}})_1(1 + a_2 + a_3) \end{aligned} \quad (18)$$

where

$$a_3 = \frac{\Pr[l_3 < d_m/l_2 < d_m, l_1 < d_m]}{\Pr[l_1 < d_m]} = \frac{(m-3)\left[4\pi(d_l + d_m)^2 - \frac{2\pi}{4}d_l^2\right]}{(m-1)[4\pi(d_l + d_m)^2]} \quad (19)$$

and l_3 = the distance between particle A and D.

By extension the interaction of one particle and n others will produce an expected excluded volume about that particle equal to

$$E(V_{\text{ex}})_n = E(V_{\text{ex}})_1(1 + a_2 + a_3 \dots + a_n) \quad (20)$$

where

$$a_n = \frac{\Pr[l_n < d_m/l_{n-1} < d_m, \dots, l_1 < d_m]}{\Pr[l_1 < d_m]} = \frac{(m-n)\left[4\pi(d_l + d_m)^2 - \frac{(n-1)}{4}\pi d_l^2\right]}{(m-1)[4\pi(d_l + d_m)^2]} \quad (21)$$

Let $\bar{V}_{\text{ex}} = E(V_{\text{ex}})_n$, the expected excluded volume between one particle and n others. After simplification of the expression for a_1 through a_n and substitution into Equation 20,

$$\begin{aligned} \bar{V}_{\text{ex}} &= E(V_{\text{ex}})_1 \left[\left(1 + \frac{m-2}{m-1} + \dots + \frac{m-n}{m-1}\right) - \frac{d_l^2}{16(d_l + d_m)^2} \frac{(m-2) + 2(m-3) + \dots + (n-1)(m-n)}{(m-1)} \right] \\ &= E(V_{\text{ex}})_1 \left[\frac{n(2m-n-1)}{2(m-1)} - \frac{d_l^2}{96(d_l + d_m)^2} \times \frac{m(n-1)(3m-2n-2)}{(m-1)} \right] \end{aligned} \quad (22)$$

The maximum number, n , of particles that can interact with a central one is readily seen to be given approximately by

$$n_{\text{max}} = \frac{4\pi(d_l + d_m)^2}{\frac{\pi}{4}d_l^2} = 16 \left(1 + \frac{d_m}{d_l}\right)^2 \quad (23)$$

It is now possible to simplify Equation 22 by substituting in Equation 23 for the value of n . If we further substitute $ddm/l_1 = \omega$, Equation 22 becomes

$$\bar{V}_{\text{ex}} = E(V_{\text{ex}})_1 \left[\frac{m}{m-1} (8.5 + 16\omega + 8\omega^2) - \frac{1}{m-1} \times (52.6 + 186.7\omega + 264\omega^2 + 170.6\omega^3 + 42.6\omega^4) \right] \quad (24)$$

For the sample containing m large particles, the total expected excluded volume is readily seen to be the sum of the expected excluded volumes about each particle less those parts which are already accounted for about another particle. The total expected excluded volume thus is

$$(V_{\text{ex}})_m = \frac{m-1}{m} \bar{V}_{\text{ex}} + \frac{m-2}{m} \bar{V}_{\text{ex}} + \dots + \frac{1}{m} \bar{V}_{\text{ex}} = \frac{m-1}{2} \bar{V}_{\text{ex}} \quad (25)$$

Substituting Equation 24 into Equation 25, we get

$$(V_{\text{ex}})_m = E(V_{\text{ex}})_1 [m(4.25 + 8\omega + 4\omega^2) - (26.3 + 93.3\omega + 132\omega^2 + 85.3\omega^3 + 21.3\omega^4)] \quad (26)$$

Up to this point, we have dealt with a sample containing m particles. Since m is not a constant in the general case, the expected excluded volume for a sample of volume V_{sa} becomes

$$E(V_{\text{ex}}) = E(V_{\text{ex}})_1 [(4.25 + 8\omega + 4\omega^2)E(m) - (26.3 + 93.3\omega + 132\omega^2 + 85.3\omega^3 + 21.3\omega^4)] \quad (27)$$

where $E(m)$ is the expected number of large particles in the sample of size V_{sa} :

$$E(m) = \frac{V_{sa}x}{V_l} \quad (28)$$

Since V_{sa} and V_l are constants,

$$\sigma_m^2 = \left(\frac{V_{sa}}{V_l} \right)^2 \sigma_x^2 \quad (29)$$

For a given mixture, $E(V_{ex})_1$ is a constant; thus, the variance of the excluded volume fraction can be obtained from Equations 27, 28, and 29 as

$$\sigma_{ex}^2 = \left[\frac{E(V_{ex})_1}{V_l} (4.25 + 8\omega + 4\omega^2) \right]^2 \sigma_x^2 \quad (30)$$

One must now consider the distribution of medium and small particles in the space remaining after the large particles have been fixed in space.

The total sample volume can be divided into three distinct subvolumes: V_l , the volume occupied by the large particles; V_{ex} , the excluded volume in which only small particles may fit; and V_{m+s} , the volume available to medium and small particles alike.

For a random mixture, the expected values of the subvolumes are

$$E(V_l) = X \cdot V_{sa}$$

$$E(V_{ex}) = E(V_{ex})_1 \left[(4.25 + 8\omega + 4\omega^2) \frac{V_{sa}X}{V_l} - \right. \quad (31)$$

$$\left. (26.3 + 93.3\omega + 132\omega^2 + 85.3\omega^3 + 21.3\omega^4) \right]$$

$$E(V_{m+s}) = E(V_{sa}) - E(V_l) - E(V_{ex}) = V_{sa}(1 - X) - E(V_{ex})$$

The expected standard deviations of the volume fractions occupied by the medium and small particles are found in a manner similar to that for the large particles. The volume in which they can be found is less than the total volume by that occupied by the large particles and by the excluded volume, so that the expected concentration of medium particles must be increased, and the variance becomes

$$\sigma_y^2 = \frac{y'(1 - y')}{b} \quad (32)$$

where

$$y' = \frac{V_{as}}{E(V_{m+s})} \quad y, \quad b = \frac{E(V_{m+s})}{V_m}$$

and y = fraction of medium particles in the mixture.

For the small particles present in V_{m+s} the standard deviation is constrained to the same value as σ_y . By definition, the excluded volume V_{ex} , consists of pockets of unmixed small particles. The total volume occupied by small particles is the excluded volume plus the volumes occupied by those in V_{m+s} . Let us denote V_{sm} as the volume of small particles in V_{m+s} . Hence, $V_s = V_{sm} + V_{ex}$, with variance

$$\sigma_z^2 = \sigma_z^2(y) + \sigma_z^2(ex) \quad (33)$$

where $\sigma_z^2(y)$ = contribution to the small particle distribution variance from volumes where medium size particles are present

$\sigma_z^2(ex)$ = contribution to the small particle distribution variance from the excluded volumes

But, since

$$\sigma_z^2(y) = \sigma_y^2$$

and

$$\sigma_z^2(ex) = \sigma_{ex}^2$$

Equation 33 becomes

$$\sigma_z^2 = \sigma_y^2 + \sigma_{ex}^2 \quad (34)$$

The expected volumes and associated values of the variances for a "random" mixture are presented in Table I. Experimentally, the expected variances can be obtained from the equations

$$\hat{\sigma}_x^2 = \frac{1}{N(N-1)} \sum (x_i - \bar{x})^2 + \frac{1}{N-1} (x - \bar{x})^2 \quad (35)$$

$$\hat{\sigma}_y^2 = \frac{1}{N(N-1)} \sum (y_i - \bar{y})^2 + \frac{1}{N-1} (y - \bar{y})^2 \quad (36)$$

$$\hat{\sigma}_z^2 = \frac{1}{N(N-1)} \sum (Z_i - \bar{Z})^2 + \frac{1}{N-1} (Z - \bar{Z})^2 \quad (37)$$

The extent of the agreement between the experimental values obtained for Equations 35, 36, and 37, and the values of the variances obtained from Equations 5, 32, and 34, respectively, should give weight to the validity of the authors' model. Some testing was done, as described below.

Table I. Expected Volumes and Variances in a Fully Mixed Mixture of Three Different Sizes, as Derived in This Paper

Particle Size	Expected Volume	Variance of Volume Fraction
Large	$(x) (V_{sa})$	$\sigma_x^2 = \frac{x(1-x)}{a}; a = V_s/v_l$
Medium	$(y) (V_{sa})$	$\sigma_y^2 = \frac{y'(1-y')}{b}; b = E(V_{m+s})/v_m$ $y' = V_{sa}/E(V_{m+s})y$
Small	$(z) (V_{sa})$	$\sigma_x^2 = \sigma_y^2 + \sigma_{ex}^2$
Excluded volume	$E(V_{ex})$	$\sigma_{ex}^2 = \left[\frac{E(V_{ex})_1}{V_l} (4.25 + 8\omega + 4\omega^2) \right]^2 \sigma_x^2$

Table II. Calculation of Standard Deviation in Silica Gel Mixing

Run No.	Size	Av. Fraction, %	$\frac{E(V_{ex})}{E(V_{ex})} + \frac{E(V_{m+s})}{E(V_{ex})}$, %	Standard Deviation, %		
				By Buslik's model	By Eqns. 5, 30, 32	From exptl. data
1	L	33.0	29.12	0.986	1.145	1.187
	M	32.5		0.690	0.7972	0.735
	S	34.5		0.654	0.7976	0.786
2a	L	33.3	28.36	0.942	1.096	0.980
	M	33.5		0.657	0.7665	0.750
2b	S	33.2		0.623	0.7669	0.820
	L	33.6	26.38	0.944	1.100	1.028
	M	33.6		0.659	0.7690	0.762
3	S	32.8		0.625	0.7694	0.870
	L	33.1	26.39	0.939	1.092	1.093
	M	33.9		0.650	0.7597	0.600
	S	33.0		0.617	0.7600	0.883

Table III. Calculation of Standard Deviation in Glass Beads Mixing

Particle Size	Av. Fraction, %	$\frac{E(V_{ex})}{E(V_{ex})} + \frac{E(V_{m+s})}{E(V_{ex})}$, %	Standard Deviation, %	
			By Eqns. 5, 30, 32	From exptl. data
-24 + 28	32.6	9.61	0.682	0.704
-32 + 35	33.7		0.543	0.226
-42 + 48	33.7		0.543	0.797

Experimental Equipment and Procedure

To test the mathematical model, graded particles were mixed in a drum mixer. The drum was made from a 9-inch length of standard 8-inch steel pipe, internally machined to a diameter of 8 inches, and split longitudinally into six identical pieces. The end plates were machined from mild steel and fastened to $\frac{5}{8}$ -inch drive shafts by means of an aluminum collar bolted to the plates. The shafts were supported by sleeve bearings placed on a wooden box.

The mixer was driven by a motor and pulley arrangement to produce a speed of 36 r.p.m. Thin steel flights were placed longitudinally in the mixer to improve mixing.

Two types of particles were used for mixing—glass beads of screen fractions $(-24 + 28)$, $(-32 + 35)$, and $(-42 + 48)$; and silica gel of screen fractions $(-14 + 16)$, $(-20 + 24)$, and $(-28 + 32)$.

As a starting condition, the drum was divided into three separate compartments by two vertical partitions parallel to the axis of the drum. For both types of mixes, equal volumes of the three different sizes were placed in the mixer, one in each of the compartments. The partitions were carefully removed after the surface was levelled, and the mixer was closed. The mixer was then run long enough for mixing to reach equilibrium. This required more than 900 revolutions. The mixer was then stopped, and 20 samples were randomly taken for analysis. Randomness of sampling was ensured by allocating numbers to 100 sectors in the mixture and selecting the sectors to sample by use of a table of random numbers (12).

A plastic scoop was used to collect the samples in each layer, and a vacuum hose was used to remove the remainder of each layer after sampling. A thin layer was then skimmed off before the next set of samples was collected. Each sample was separated into its three component sizes by screening, and the size fractions were separately weighed to the nearest 0.1 mg. The experimental standard deviations were then calculated by Equations 35, 36, and 37.

Results and Discussion

Table II compares the standard deviations calculated from Equations 5, 33, and 34 with the standard deviations by Buslik's formula and the experimental data for three runs using silica gel particles.

In both theoretical and experimental evaluations of standard deviation, uniform density is assumed throughout the mixture, and the packing effect is considered. The packing effect gives the ratio of the volumes before and after packing to be 1.16.

A series of runs was made using the glass beads with various sizes of flights. The results obtained are shown in Table III for comparison. The differences in theoretical and experimental values of σ_s' in Table II are small while the differences for σ_y and σ_z in Table III are much greater. These larger discrepancies in Table III are due to apparent inability to mix smooth spheres completely. In Table III, the estimate of the standard deviation for the medium particles is much less than the theoretical, and for the small particles is substantially more than the theoretical value. This fact was characteristic of the bad mixtures made, whether with glass beads or silica gel, and is perhaps an index of poor mixing far more sensitive than the estimated large particle standard deviation.

The equations developed in this paper agree with the experimental results significantly better than do those from Buslik's model. Analysis using the F-test (l, δ) shows no significant difference between the experimental results for the silica gel mixes and the calculated values. On the other hand, Buslik's

calculated variance for the small size particles was different from the experimental results with 98% confidence. The F-test on the two models showed significantly different variances for all particle sizes.

The method above was presented for three sizes of particles. To extend the method to more than three sizes, one must consider the excluded volumes between all particles larger than the one under consideration. Thus, if one were to consider particles of size 4, where particles of size 1, 2, and 3 are larger, the interactions that result in excluded volumes are between 1-1, 1-2, 1-3, 2-2, 2-3, and 3-3. If the mixture under study contains n distinct sizes, the total number of contributions to the excluded volumes will be:

$$\sum_{j=1}^{n-2} \left(\sum_{i=0}^j i \right)$$

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The problem of defining a mixture of multi-sized solids was brought to the attention of one of the authors while working in the Chemical Engineering Division of the Atomic Energy Research Establishment, Harwell, England. The discussions with P. M. Lacey were particularly helpful in bringing out the main difficulties involved.

Nomenclature

A, B, C	= weight fractions
a	= V_{sa}/V_l
a_2, a_3, \dots, a_n	= correction factors
b	= $E(V_{m+s})/v_m$
d_l, d_m	= diameter of a large and medium particle, respectively
$E(V_{ex})$	= expected value of V_{ex}
$E(V_{ex})_n$	= expected value of the excluded volume between $(n - 1)$ large particles and one fixed large particle
$E(V_{m+s})$	= expected value of V_{m+s}
$f(l)$	= probability density function of l
$F(l)$	= distribution function of l
l	= distance between two large particles
m	= number of large particles in a sample
N	= number of samples analyzed in a mixture
n	= number of particles in a sample
n_{max}	= maximum number of large particles around a central one
P	= fraction of a component in the mixture
P_i	= binomial distribution probability
r_l, r_m	= radius of a large and medium particle, respectively
s	= weight fraction of large particles
V_{ex}	= excluded volume
V_l	= volume of large particles
V_{m+s}	= volume available to medium and small particles alike
V_0	= constant
V_{sa}	= sample volume
v_l, v_m, v_s	= volume of a large, medium, and small particle, respectively
W	= weight of a sample
w	= weight of a particle
\bar{w}	= average particle weight in the whole mixture
x, y, z	= volume fraction of large, medium, and small particles in a mixture, respectively
$\bar{x}, \bar{y}, \bar{z}$	= mean fraction of large, medium, and small particles in N samples, respectively
x_i, y_i, z_i	= fraction of large, medium, and small particles in i th sample
y'	= modified function of medium particles
σ	= standard deviation
σ_{ex}^2	= variance of the excluded volume fraction
σ_m^2	= variance of a number of large particles in the samples
$\sigma_{x_i}^2, \sigma_{y_i}^2, \sigma_{z_i}^2$	= variance, of large, medium, and small particles, respectively

σ_{x+y}^2 = variance of large and medium particles together
 $\sigma_z^2(\text{ex})$ = contribution to variance of small particles from the excluded volume
 $\sigma_z^2(y)$ = contribution to variance of small particles from volume where medium size particles may be present
 $\hat{\sigma}_{x_i}^2, \hat{\sigma}_{y_i}^2, \hat{\sigma}_z^2$ = estimated variance of large, medium, and small particles in the mixture, respectively
 ω = the ratio dm/d_i

Literature Cited

- (1) Bennett, C. A., Franklin, N. L., "Statistical Analysis in Chemistry and the Chemical Industry," pp. 319-23, New York, 1954.
- (2) Blumberg, R., Maritz, J. S., *Chem. Eng. Sci.* **12**, 240 (1953).
- (3) Brothman, A., Wollan, G. N., Feldman, S. M., *Chem. Met. Eng.* **52**, 102 (1945).

- (4) Buslik, D., *ASTM Bull.* No. **66**, April, 1950.
- (5) Coulson, J. M., Maitra, N. K., *Ind. Chemist* **26**, 55 (1950).
- (6) Davies, O. L., "Statistical Methods in Research and Production," 3rd ed., pp. 368-71, London, 1958.
- (7) Hemelrijk, J., "Statistical Methods Applied to the Mixing of Solid Particles," *Math. Centrum Bull.* **S159**, Amsterdam, 1954.
- (8) Lacey, P. M. G., *Trans. Inst. Chem. Engrs., London* **21**, 52 (1943).
- (9) Manning, S. B., *J. Inst. Fuel* **56**, 153 (1937).
- (10) Mayagi, S., *J. Ceram. Assoc. Japan* **58**, 417 (1950).
- (11) Oyama, Y., *Sci. Papers Inst. Phys. Chem. Res. (Tokyo)* **37**, 951 (1940).
- (12) Rand Corp., "A Million Random Digits with 100,000 Normal Deviates," Free Press, Glencoe, Ill., 1955.
- (13) Stange, K., *Chem. Eng. Tech.* **26**, 331 (1954).
- (14) Weidenbaum, S. S., Bonilla, C. F., *Chem. Eng. Progr.* **51**, 27-J (1955).

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